



Constructing hollow porous Pd/H-TiO₂ photocatalyst for highly selective photocatalytic oxidation of methane to methanol with O₂

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ABSTRACT

The partial oxidation of methane to methanol with O₂ is an attractive catalytic reaction, but the catalysts still face great challenges in terms of activity and selective oxidation, especially how to avoid overoxidation. Herein, Pd/H-TiO₂ with a unique hollow porous nanocage structure was prepared for selective photooxidation of methane into methanol by O₂ under mild conditions. The as-obtained Pd/H-TiO₂ exhibited a high methanol production rate of 4.5 mmol/g/h with selectivity reaching up to 70 % under optimized conditions, exceeding most reported values. The mechanism study indicated that •OH radicals, produced by photogenerated holes, played an important role in the activation of methane into •CH₃ species, and the latter was further oxidized into methanol by •O₂ radicals formed by photogenerated electrons. The strong metal-support interaction and unique porous hollow structure also effectively enhanced the catalytic activity. These new insights provide us guidance for the design of high-performance photocatalysts for selective photocatalytic oxidation of methane.

1. Introduction

Methanol is an important liquid fuel and feedstock for the manufacture of olefins, aromatics, and other fine chemicals. And it also could replace fossil fuels as an alternative energy source in energy storage and ground transportation, leading to a feasible “methanol economy” [1–3]. However, large-scale transformation of methane into methanol is usually based on an energy-intensive indirect conversion process via firstly producing synthesis gas (> 700 °C) under high temperatures and pressures [4–7]. Therefore, direct selective oxidation of methane to methanol under mild conditions is very attractive, thereby called by the “Holy Grail” reaction [6,8–13].

Among processes, photocatalysis may easily activate the first C–H bond in methane, thereby converting methane into methanol at low temperatures or even room temperature [14–21]. However, the grand challenge of photocatalysis is to achieve high activity and selectivity of methanol at the same time [22–24]. Although high yields of liquid products can be obtained, avoiding the formation of by-product formaldehyde (HCHO) and methyl peroxide (CH₃OOH) is still quite difficult, leading to the poor selectivity of methanol [25]. Additionally, H₂O₂ is

used as an oxidant in most photocatalytic systems, resulting in the high cost and low economic value [26]. In this regard, molecular oxygen (O₂) is more ideal for the oxidation of methane but much more difficult to activate CH₄ than H₂O₂ [27,28]. Therefore, the photocatalytic oxidation of methane using O₂ as the oxidant to achieve a high yield and methanol selectivity simultaneously is still challenging to date.

TiO₂ is a classic semiconductor photocatalyst that attracted extensive attention in the photooxidation of methane [29,30]. Various strategies have so far been proposed to improve the yield and selectivity of methanol and achieve desired catalysis efficiency, such as loading metal nanoparticles (NPs) as co-catalysts and engineering surface structure over TiO₂ based catalysts [16,25,31]. Thereinto, the hollowing structure has attracted intense attention in TiO₂ based photocatalysis since it can improve light scattering, reduce charge migration distance, and decline direct charge separation to endow photocatalysts with excellent photocatalytic performance [32,33]. In this work, hollowing strategy and loading metal co-catalysts are combined to synthesize high-performance TiO₂ based photocatalyst. Specifically, hollow porous TiO₂ (H-TiO₂) nanocages were prepared through the pyrolysis of Ti-based MOF (MIL-125-NH₂) and Pd NPs as co-catalysts were loaded onto H-TiO₂ by a

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photochemical route. The resulting Pd/H-TiO₂ showed excellent performance toward photocatalysis of methane oxidation with molecular oxygen. Under the optimized condition (3 MPa), the methanol production rate over Pd/H-TiO₂ reached 4.5 mmol/g/h and selectivity attained 70 %, superior to most reported values. The mechanism study demonstrated that the unique hollow structure and strong metal-support interaction of Pd/H-TiO₂ synergistically promoted the photocatalytic performance.

2. Experimental

2.1. Chemicals and materials

Chloroauric acid (HAuCl₄·4H₂O, 99.9 %), Pd chloride (II) (PdCl₂, 99.9 %), chloroplatinic acid (H₂PtCl₆·6H₂O), silver nitrate (AgNO₃ 99.8 %), N, N-dimethylformamide (DMF, 99.5 %) and methanol (99.5 %) were purchased from Sinopharm Chemical Reagent Co., Ltd. Titanium (IV) isopropoxide (C₁₂H₂₈O₄Ti, 99 %), polyvinyl pyrrolidone (PVP, K30), and 2-aminoterephthalic acid (H₂ATA, 98 %) were purchased from Energy Chemical. All chemicals were analytical graded and used without further purification.

2.2. Material synthesis

2.2.1. Synthesis of MIL-125-NH₂

First, 75 mg H₂ATA was dispersed in a mixture of 7 mL DMF and 3 mL methanol. Then, 75 μ L C₁₂H₂₈O₄Ti was added to the reaction mixture and sonicated for 5 min. Next, the above mixture was transferred into a 25 mL Teflon-lined stainless-steel autoclave and heated at 150 °C for 24 h. The obtained product was centrifuged, washed several times with ethanol, and finally dried in an oven overnight at 60 °C.

2.2.2. Synthesis of H-TiO₂

500 mg of MIL-125-NH₂ precursor was placed in a porcelain boat and calcined by a muffle furnace with the ramp of 1 °C/min to 500 °C for 4 h.

2.2.3. Syntheses of metal (Pd, Pt, Au, Ag)/H-TiO₂ and Pd/C-TiO₂

2.2.3.1. Pd/H-TiO₂. 30 mg prepared H-TiO₂ and 20 mg PVP were added to a mixed solution of 30 mL of H₂O and 1 mL of methanol. And 200 μ L H₂PdCl₄ (1 mg_{pd}/mL) was added into the above solution. The mixture was irradiated by a 300 W Xe lamp equipped with a UV filter (λ < 400 nm) for 2 h under stirring. The sample was centrifuged, washed with ethanol for several times, and finally dried in an oven overnight at 60 °C.

2.2.3.2. Metal (Pt, Au, Ag)/H-TiO₂. The H₂PdCl₄ was changed into H₂PtCl₆·6H₂O, HAuCl₄·4H₂O, and AgNO₃ with the same metal content. The other steps were the same as Pd/H-TiO₂.

2.2.3.3. Pd/C-TiO₂. H-TiO₂ was changed into commercial TiO₂ (anatase crystal structure). The other steps were the same as Pd/H-TiO₂.

2.2.4. Synthesis of Pd + H-TiO₂

0.2 mg Pd black and 30 mL H-TiO₂ were dispersed into 30 mL H₂O. And the mixed solution was stirred for 4 h. The sample was centrifuged and washed with ethanol for several times and the resulting powder was dried in an oven overnight at 60 °C.

2.3. Characterization of samples

The morphology and structure of as-prepared catalysts were measured by scanning electron microscope (SEM, Hitachi S4800). High-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) and energy dispersive X-ray spectroscopy (EDS)

were measured on transmission electron microscope (TEM, Tecnai F30) with an accelerating voltage of 300 kV. The crystal phase of as-prepared products was determined by powder X-ray diffraction (XRD, Rigaku Ultima IV X-ray diffractometer) with Cu K α radiation (λ = 1.54056 Å). The precise contents of metal elements in samples were determined by inductively coupled plasma-mass spectrometry (ICP-MS, Agilent 7700x). Electron paramagnetic resonance (EPR) spectra were obtained by using Bruker X-band A200. X-ray photoelectron spectroscopy (XPS) was measured on the PHI Quantum-2000 system, and a monochromatic aluminum anode with K α radiation (1486.6 eV) was used as the X-ray source. All XPS spectra were calibrated with the C1s peak at 284.8 eV as the internal standard. Solid UV-vis absorption spectra were measured on Carry 5000. *In situ* diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) was tested on an infrared spectrometer (NICOLET 6700), in which a 300 W Xe lamp (equipped with 420 nm band pass filter) was employed as light source.

2.4. Catalytic tests

The performances of samples on photocatalytic oxidation of methane were evaluated in a commercial evaluation system (CEL-HPR100T+, Beijing China Education Au-Light Co., Ltd). First, 10 mg catalyst was dispersed in a quartz lining filled with 60 mL H₂O and transferred into the bottom of a stainless-steel reactor with a quartz window (diameter: 3.5 cm). After being sealed, the reactor was flushed several times to remove the air and then filled with 2 MPa CH₄/O₂ mixed gas (CH₄:98 %, O₂:2 %). Next, the reactor was irradiated by a 300 W Xe lamp (PLS-SXE300D, Perfectlight.cn.). The final products were detected by gas chromatography (SHIMADZU GC-2014C) equipped with a flame ionization detector and thermal conductivity detector. The liquid phase product was detected by 500 M NMR (AVANCE III HD 500 MHz), and dimethyl Sulfoxide (DMSO) diluted 10,000 times was added as an internal standard. For detecting HCHO, the reagent aqueous solution was prepared by dissolving 15 g ammonium acetate, 0.3 mL of acetic acid, and 0.2 mL of pentane-2,4-dione in 100 mL water. Then, 0.5 mL of liquid product was mixed with 1.0 mL of water and 0.5 mL of reagent solution. The mixed solution was maintained at room temperature for 3 h and measured the absorption intensity at 413 nm by UV-vis absorption spectroscopy.

2.5. In situ DRIFT

The catalyst powder was placed in the DRIFTS cell. He (99.9995 %) was used to purge the cell for 30 min. After that, the CH₄/O₂ mixed gas (CH₄:98 %, O₂:2 %) was introduced through a glass tube filled with H₂O for 30 min. Light was then introduced through the window of the cell and the data was collected every 10 min.

2.6. In situ EPR

5 mg Pd/H-TiO₂ was dispersed in 5 mL aqueous solution. And CH₄/O₂ gas mixture was bubbled into the above solution for 20 min. Take 200 μ L of the mixture and add 40 μ L of 5,5-dimethyl-1-pyrroline N-oxide (DMPO). Then, Xe lamp irradiation was introduced and detected the signal at 5 min, 10 min and 15 min. For detecting \bullet O₂, the Pd/H-TiO₂ was dispersed in 5 mL of methanol solution. And O₂ gas was bubbled into the above solution for 20 min. Other steps were the same as above to detect \bullet OH.

3. Results and discussion

3.1. Catalyst characterizations

The synthesis process of Pd/H-TiO₂ is schematically illustrated in Fig. 1a. First, MIL-125-NH₂ precursors shaped as square bricks with side length of about 800 nm and thickness of about 300 nm were synthesized

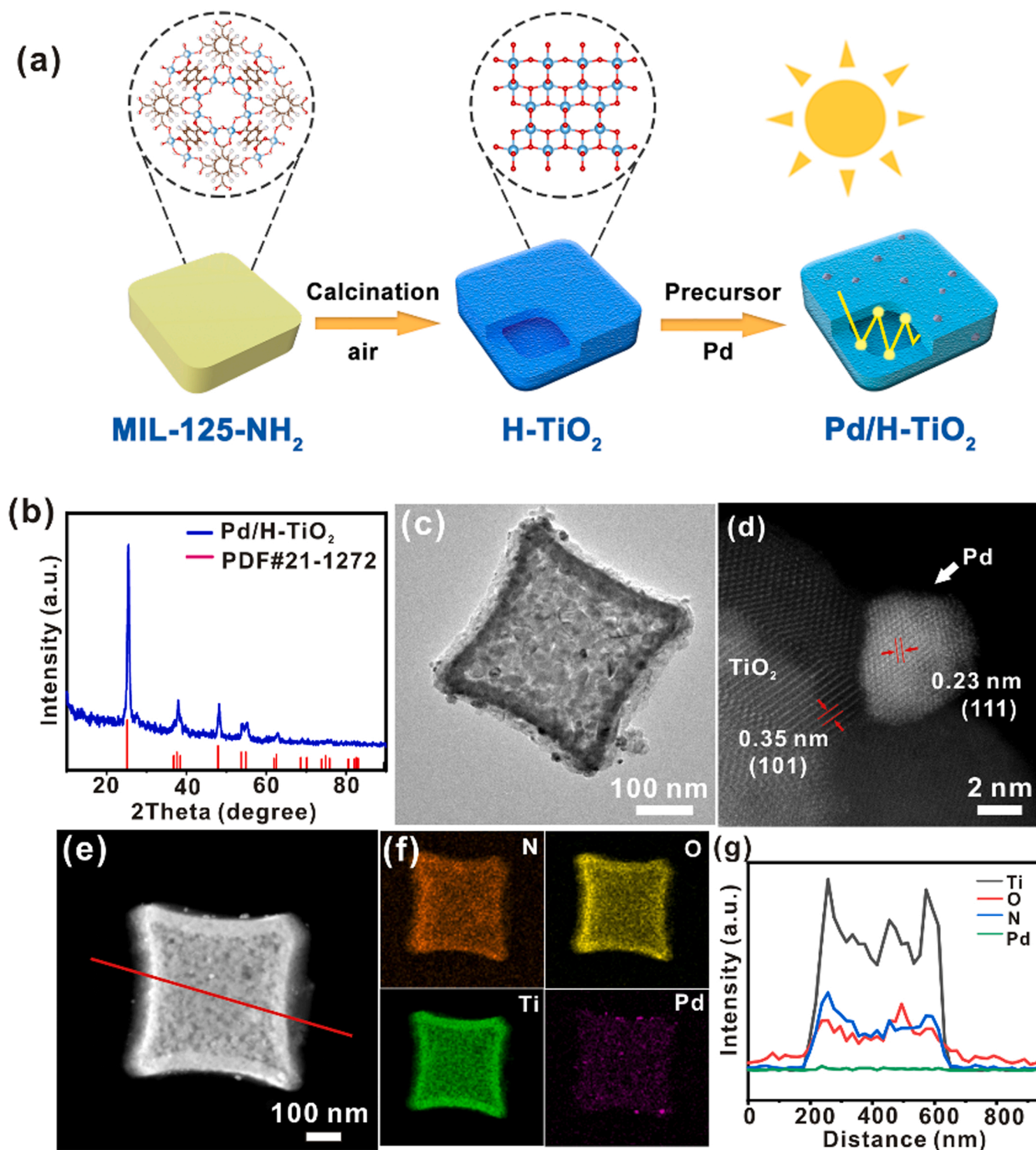


Fig. 1. (a) Scheme illustrating the synthesis of Pd/H-TiO₂ with the architecture of porous nanocage. (b) XRD pattern of Pd/H-TiO₂, (c) low-magnification TEM image of individual Pd/H-TiO₂ nanocage and its local HRTEM image, (d-f) HAADF-STEM image and corresponding EDS maps of individual Pd/H-TiO₂ nanocage, (g) EDS elemental line profiles of Pd/H-TiO₂ along the red line in (e).

by a hydrothermal route (Fig. S1). Next, MIL-125-NH₂ precursors were calcined in the muffle furnace at 500 °C for 4 h to form a hollow TiO₂ structure (H-TiO₂). As shown in Fig. S2, the products after calcination maintained the morphology of square brick. However, TEM observation revealed a transformation into a hollow structure with a wall thickness of 40–50 nm (Fig. S3). The adsorption/desorption isotherm measurement revealed that H-TiO₂ exhibited obviously mesoporous characteristics and its specific surface area reached 16 m² g⁻¹ (Fig. S4). Finally,

Pd NPs were loaded onto H-TiO₂ through a facile photochemically reduction route to form Pd/H-TiO₂ (Fig. S5).

The powder XRD pattern of the as-synthesized Pd/H-TiO₂ is displayed in Fig. 1b. Only peaks of anatase TiO₂ were observed due to the low content of Pd, determined as only 0.52 wt% by ICP-MS. As revealed by TEM (Fig. 1c), some Pd NPs of 5–10 nm with deeper contrast randomly decorated the surface of hollow TiO₂ nanocages. The corresponding HRTEM image (Fig. 1d) further confirmed well-crystallized Pd

NPs and H-TiO₂ with very strong contact between both. A clear Pd/TiO₂ interface was observed, in which the lattice fringes of 0.35 nm and 0.23 nm corresponded to TiO₂ (101) plane and Pd (111) plane, respectively. Of note, HAADF-STEM image and corresponding EDS elemental maps of Pd/H-TiO₂ (Fig. 1e–f) revealed that N atoms from -NH₂ group were doped into the lattice of H-TiO₂ during pyrolysis of MIL-125-NH₂. The EDS elemental line profiles of Pd/H-TiO₂ further verified catalyst exhibiting a unique hollow structure (Fig. 1g). The solid UV–vis absorption spectra (Fig. S6) illustrated an absorption edge of H-TiO₂ around 416 nm, corresponding the band gap of 2.98 eV by the Tauc's plots [34]. After loading Pd nanoparticles, the band gap of Pd/H-TiO₂ decreases to 2.68 eV, indicating the formation of a metal-semiconductor heterojunction. Of note, the light absorption ability of the catalyst in the visible range was significantly enhanced after loading of H-TiO₂ with Pd NPs. Obviously, the enhanced light absorption would be beneficial to the improvement of photocatalytic performance.

3.2. Catalytic performances

The performance of Pd/H-TiO₂ toward the photocatalytic oxidation of methane in the presence of O₂ (2 %) was tested. For comparative purposes, Au/H-TiO₂, Pt/H-TiO₂, and Ag/H-TiO₂ with Au, Ag, and Pt NPs loaded onto H-TiO₂ were also synthesized by the same method and metal contents to serve as control catalysts (Fig. S7–8). The detailed properties of relevant catalysts are summarized in Table S1. As shown in Fig. 2a, the H-TiO₂ has the ability to convert methane into CO₂, CH₃OOH, HCHO, and CH₃OH. However, both the production rate (0.18 mmol/g/h) and selectivity (9.2%) of methanol were very low. By contrast, all M/H-TiO₂ (M = Au, Ag, Pd, and Pt) showed significantly improved activity and selectivity. Among M/H-TiO₂ catalysts, Pd/H-TiO₂ exhibited the best performance in converting CH₄ into methanol. The production rate of methanol over Pd/H-TiO₂ reached 2.4 mmol/g/h

h, a value 13-fold that of H-TiO₂. Also, the selectivity of methanol significantly increased from 9.2 % to 54.8 %. In our experiments, the concentration of methanol was determined by ¹H NMR spectroscopy and the concentration of HCHO in liquid products was measured by the acetylacetone color method (Fig. S9–11). The results also show that the M/TiO₂ heterostructure effectively enhanced the methane conversion rate. However, various metals played a distinct effect on product selectivity. For Au/H-TiO₂ and Ag/H-TiO₂, loading of Au and Ag NPs enhanced the yield of liquid products, but avoiding the formation of HCHO and CH₃OOH by-products was still challenging, thereby leading to the low methanol selectivity of 28.9 % and 24.6 %, respectively. Note that CH₃OOH can be obtained in the liquid products over Au/H-TiO₂ and Ag/H-TiO₂, different from Pt/H-TiO₂ and Pd/H-TiO₂. The reason for this may have to do with Pd and Pt NPs as co-catalysts, which exhibited a relatively higher activity to convert important intermediates of CH₃OOH into CH₃OH [35].

In order to explore the influence of metal deposition methods, other control catalysts were also prepared by physically mixing and H₂ reduction (denoted as Pd + H-TiO₂ and Pd/H-TiO₂(H₂), respectively). The HAADF-STEM images indicated no obvious Pd-TiO₂ interface in Pd + H-TiO₂, and Pd/H-TiO₂(H₂) showed smaller sized Pd NPs (Fig. S12). The methanol production rates over Pd + H-TiO₂ and Pd/H-TiO₂(H₂) were 0.42 mmol/g/h and 0.65 mmol/g/h, respectively, which were much lower than that of Pd/H-TiO₂ (Fig. 2b). In addition, for the Pd + H-TiO₂ and Pd/H-TiO₂(H₂), HCHO and CH₃OOH were the main liquid products, and methanol selectivity were only 17.8 % and 20.2 %, respectively. Thus, the difference in the interaction between Pd and H-TiO₂ caused by different deposition methods significantly affected the catalytic process. Commercial anatase TiO₂ with a low specific surface area (4.9 m² g⁻¹) was then used for comparison to explore the impact of H-TiO₂ hollow structure on photocatalytic performance (denoted as Pd/C-TiO₂, Fig. S12–13). The data revealed methanol production rate over

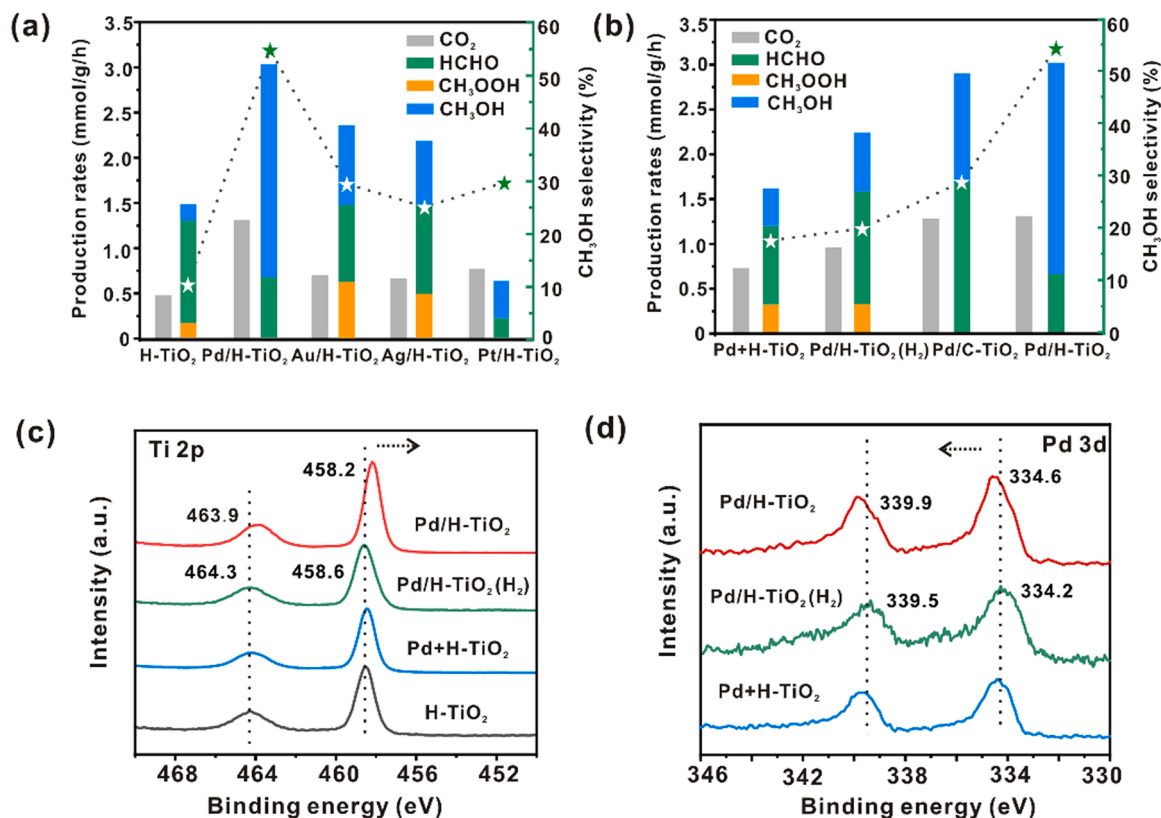


Fig. 2. Production rates obtained by the prepared catalysts: (a) H-TiO₂ and when loaded with different metals, (b) different metal deposition methods on various TiO₂ support. Reaction conditions: 10 mg cat., 60 mL water, 2 MPa, CH₄:O₂ 50:1, 45 °C, and light source of 300 W Xe lamp, 350–780 nm and 1.0 W/cm². (c) Ti 2p high-resolution XPS spectra of related samples. (d) Pd 3d high-resolution XPS spectra of related samples.

Pd/C-TiO₂ reaching 1.2 mmol/g/h, a value only half that of Pd/H-TiO₂. Also, the methanol selectivity was estimated to 29.2 %, a value much lower than that of Pd/H-TiO₂ (54.8 %). Clearly, the unique porous hollow structure of H-TiO₂ induced better catalytic performance due to the porous hollow structure conducive to improving light scattering, reducing charge migration distance, and directing charge separation [33].

Based on the above results, it can be seen that the interaction between Pd and H-TiO₂ played a key role in promoting the photocatalytic activity and selectivity. To figure out the reasons, XPS analysis was conducted to explore the electronic structures of related catalysts. In the Ti 2p high-resolution XPS spectra, the peaks of Pd/H-TiO₂ shifted to lower binding energies (0.4 eV) when compared to H-TiO₂ (Fig. 2c). Similar phenomenon was also observed in the O1s high-resolution XPS spectra of Pd/H-TiO₂ (Fig. S14). However, the binding energies of Ti 2p

and O1s in Pd + H-TiO₂ and Pd/H-TiO₂(H₂) were almost the same as those of H-TiO₂. In addition, the binding energies of Pd 3d in Pd/H-TiO₂ shifted to higher energies (0.4 eV) when compared to Pd + H-TiO₂ and Pd/H-TiO₂(H₂), indicating electrons transfer from Pd to H-TiO₂ (Fig. 2d). Therefore, Pd/H-TiO₂ possessed stronger metal-support interaction than Pd + H-TiO₂ and Pd/H-TiO₂(H₂), beneficial to the transfer of photogenerated electrons during photocatalysis. The EPR spectra of H-TiO₂, Pd/H-TiO₂ and Pd/H-TiO₂ (H₂) during reaction were tested. The results showed that the generation rate of active specie •OH was increased after loading Pd during reaction, but the photo-deposition method (Pd/H-TiO₂) was significantly better than that of H₂ reduction (Pd/H-TiO₂ (H₂)) due to stronger metal-support interaction (Fig. S15.). In addition, photoluminescence (PL) and photocurrent spectra were measured to study the separation of photogenerated charges and the results are shown in Fig. S16. The lower PL peak intensity of Pd/H-TiO₂

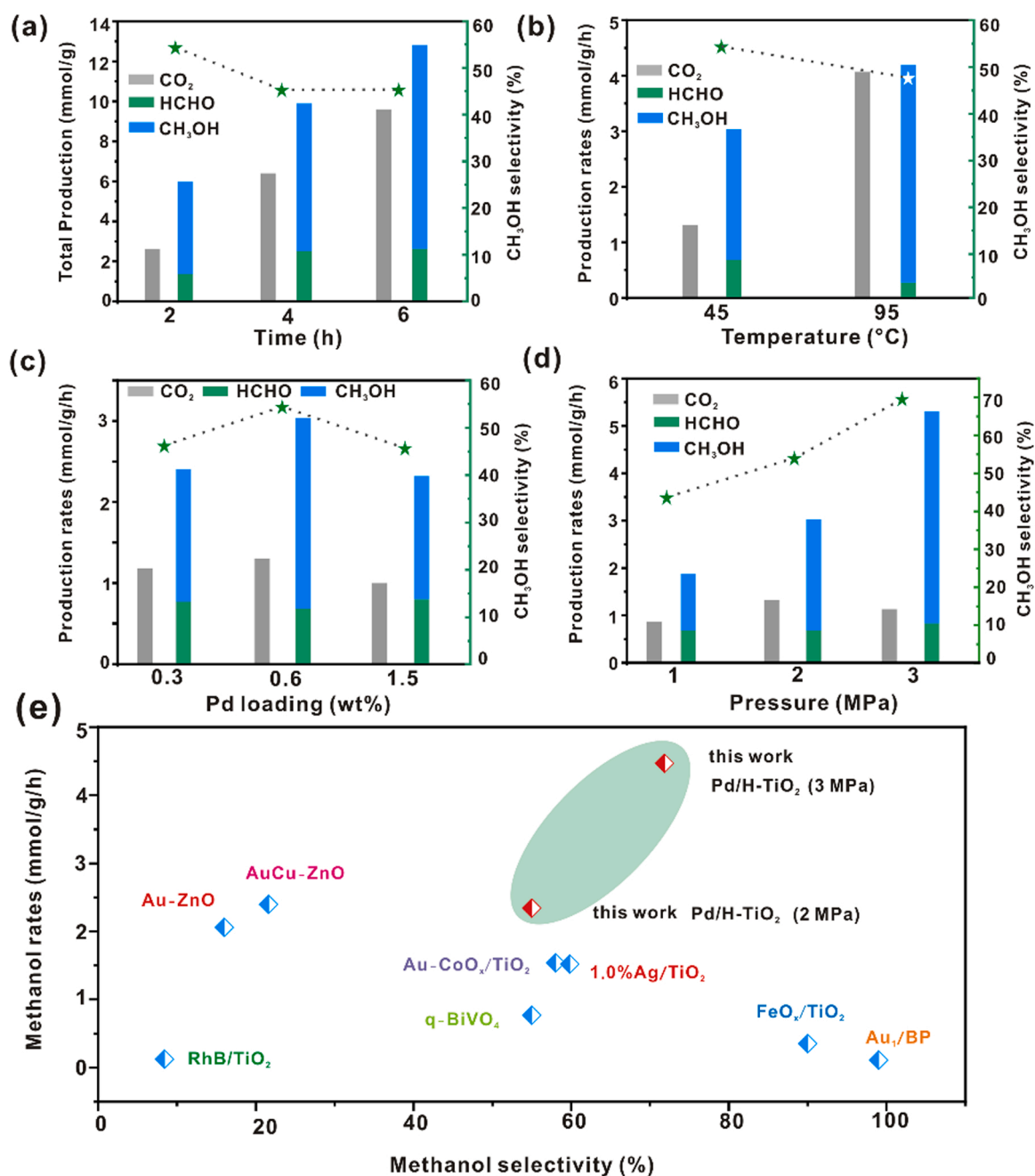


Fig. 3. (a) Dependence of methane oxidation over Pd/H-TiO₂ with irradiation time. (b–d) Production rates over Pd/H-TiO₂ at different temperatures, Pd loading amounts, and pressures. (e) Performance comparison of Pd/H-TiO₂ with other catalysts under similar conditions.

suggested that loading Pd particles helps to suppress recombination of photogenerated charges. In addition, Pd/H-TiO₂ also exhibited a higher photocurrent response compared with H-TiO₂, indicating faster and more efficient separation of photogenerated charges.

The catalytic performance of Pd/H-TiO₂ was further optimized under different conditions. To this end, catalytic tests were performed with different times (2, 4, and 6 h). As shown in Fig. 3a, the production of methanol increased with the irradiation time, while the selectivity decreased slightly. This was mainly attributed to the problem of the batch reaction system, where the produced methanol remained in the reactor and thus were easily oxidized further. Despite all this, the selectivity of methanol was still above 45 % after 6 h reaction. The rise in reaction temperature from 45 °C to 95 °C led to the enhanced production rate of methanol by 1.6-fold, while selectivity slightly dropped from 54.8 % to 47.5% (Fig. 3b). The above results revealed that increasing the reaction time and temperature can indeed promote the conversion of methane, but at the same time, it intensified the excessive oxidation of methanol to CO₂, resulting in unsatisfactory selectivity. The loading amount of Pd NPs in Pd/H-TiO₂ catalyst was also optimized, and the results showed a volcanic curve (Fig. 3c). The catalytic performance of 0.6 wt% Pd/H-TiO₂ was better than those of 0.3 wt% and 1.5 wt% Pd/H-TiO₂ (Pd loading as feeding content). In addition, the catalytic performances were tested under different pressures from 1 MPa to 3 MPa (Fig. 3d). The production rate and selectivity of methanol increased obviously with pressure. Under 3 MPa, the production rate of methanol over Pd/H-TiO₂ reached 4.5 mmol/g/h and selectivity was up to 70 %. We also evaluated the catalytic performance over Pd/H-TiO₂ at different water amounts (20, 40, and 60 mL) (Fig. S17). The results show that the yield and selectivity of liquid products significantly increased with higher water amount. The results show that increasing water amount and pressure are effective methods to improve methanol yield and selectivity, possibly by increasing the solubility of methane. The TEM and XRD of used Pd/H-TiO₂ were also characterized in Fig. S18. The results show that the structure of catalyst was still maintained after the reaction, indicating that it has a good structure stability. To better evaluate the photocatalytic performance of Pd/H-TiO₂, the results were also compared with typical catalysts reported in the literature. In Table S2, even though some reported catalysts exhibited high selectivity of oxygenate, the selectivity to target product methanol was still low. Additionally, achieving a high production rate and high selectivity of methanol at the same time was rarely reported. In this regard, Pd/H-TiO₂ are far superior to most reported catalysts (Fig. 3e). The strong interaction between Pd NPs and H-TiO₂ coupled with the unique hollow porous structure synergistically promoted the partial photo-oxidation of methane to methanol.

3.3. Mechanism analysis

Since the photooxidation of methane involves various active species, obtaining a unified reaction pathway is difficult due to similarities between reaction intermediates. For example, intermediate hydroxyl radicals may directly react with methyl groups to form methanol or may act as reactive species to activate C-H in methane [35]. To gain a better understanding of the catalytic process, various blank experiments with different reactants were conducted and the data are gathered in Fig. S19. When the reactants were changed to O₂ and water, no product was observed, indicating that methanol did not originate from contaminants. Not only that, methanol cannot be produced from the reaction between CH₄ and H₂O, suggesting the crucial role of O₂ in promoting the conversion of methane to methanol [36,37].

To further explore the reaction mechanism, multiple monitoring technologies, including *in-situ* EPR, *ex situ*-XPS, and *in-situ* DRIFT were used to detect the reaction intermediates. *In-situ* EPR can effectively detect reactive oxygen species (ROS) during the photocatalytic process. The irradiation of the reaction aqueous solution dissolving CH₄ and O₂ in water generated obvious equidistant quartet signals, belonging to

•OH radicals with intensity increasing with extending irradiation time (Fig. 4a). When the *in-situ* EPR measurement was performed in methanol aqueous solution dissolving O₂, signals assigned to superoxide anion (•O₂⁻) were detected, and the intensity increased with the irradiation time (Fig. 4b). Thus, it can be deduced that •O₂⁻ and •OH were the two main ROS in photocatalytic methane oxidation.

Further trapping experiments were also performed to determine the roles of these radicals in the selective oxidation of CH₄. Here, para-quinone and salicylic acid were added into reaction solution as sacrificial agents of •O₂⁻ and •OH, respectively (Fig. 4c). As shown in Fig. 4c, methanol was no longer produced after the addition of para-quinone or salicylic acid. It can be seen that •O₂⁻ and •OH played an indispensable role in the reaction process. To illustrate the origin of oxygen in methanol, the isotope experiment (¹⁸O₂) was performed. The results proved that oxygen in methanol was mainly derived from O₂ (Fig. S20). However, when •OH was trapped by salicylic acid (Fig. S21), methanol cannot be achieved anymore. That means that •OH play an important role to abstract H from methane to form •CH₃ [35]. Methanol was also not observed after trapping •O₂⁻, indicating that •O₂⁻ mainly promoted •CH₃ radicals into methanol, which is consistent with isotope experiments.

Ex-situ XPS was carried out to analyze C species and metal valence of catalysts during reactions. Through deconvolution, it was found that O=C-O (287.3 eV), which was an important intermediate for the over-oxidation of methane to CO₂, rose significantly after illumination (Fig. 4d) [38]. Furthermore, large numbers of oxygen vacancies were generated on the surface of TiO₂ under illumination. Accordingly, the valence of Ti then decreased, consistent with the lower binding energy of Ti 2p in Fig. 4e. By contrast, the binding energy of Pd 3d did not change under illumination, suggesting Pd NPs in Pd/H-TiO₂ remained in the metallic state (Fig. S22).

In-situ DRIFT was also conducted to observe the reaction intermediates over Pd/H-TiO₂. As provided in Fig. S23, the intensities of CO₂ peaks at 2356 cm⁻¹ and 2339 cm⁻¹ significantly increased as a function of illumination time, directly proving the occurrence of photocatalytic methane conversion. In addition, a new band appeared at 2888 cm⁻¹ under light illumination, assigned to the stretching vibration of the C-H bond of methoxy groups [25]. Meanwhile, overoxidation products were detected at 1721, 1615, and 1481 cm⁻¹, which are attributed to ν(CO) stretching of adsorbed CH₂O*, HCOO*, and δ(CH₂) of H₂COO* species, respectively [39].

Based on these results, the oxidation mechanism of methane to methanol over Pd/H-TiO₂ was extracted and schematically summarized in Fig. 4g. In this process, Pd/H-TiO₂ was first excited to generate electron-hole pairs under illumination (1). The H₂O was then oxidized by holes to produce •OH radicals (2), and O₂ was reduced by electrons to O₂⁻ (3). Next, •OH activated CH₄ to generate •CH₃ (4). Isotope experiments and trapping experiments proved that the oxygen in methanol was derived from O₂ not H₂O. Therefore, the main reaction pathway consisted of •CH₃ reacting with O₂ to form CH₃OOH, which then was converted to methanol (5). In this way, Pd/H-TiO₂ simultaneously achieved high-yield and selective photocatalytic conversion of methane to methanol.

4. Conclusions

Hollow porous Pd/H-TiO₂ nanocages were obtained by pyrolysis of MIL-125-NH₂ followed by photodeposition. Under the optimized conditions, Pd/H-TiO₂ achieved a high methanol production rate of 4.5 mmol/g/h with selectivity as high as 70 %, exceeding most literature reports. The excellent performance was related to the unique hollow porous structure, suitable Pd co-catalyst, and strong interaction between Pd and TiO₂ constructed by photodeposition. Furthermore, a deeper understanding of the catalytic mechanism was obtained by *in-situ* ESR, *ex-situ* XPS, and *in-situ* DRIFT. The results showed •OH and •O₂⁻ as the main active species involved in the photocatalytic process. Among

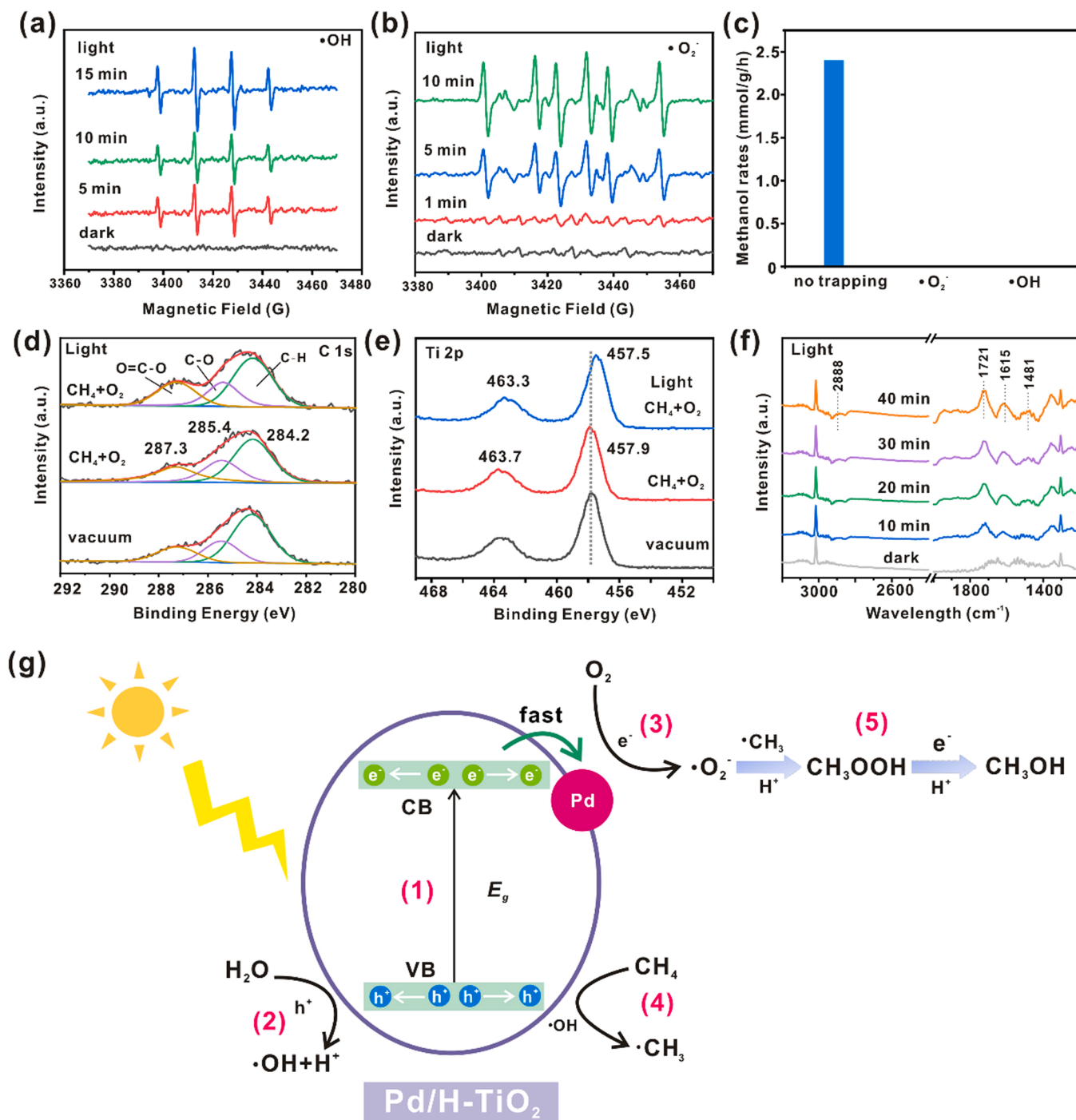


Fig. 4. In-situ EPR spectra of Pd/H-TiO₂ obtained by: (a) dissolving CH₄ and O₂ in water with different light illumination times, (b) dissolving O₂ in CH₃OH aqueous solution with different light illumination times. DMPO is used as the radical trapping agent. (c) Changes in products of CH₄ oxidation after the addition of scavengers para-quinone and salicylic acid in the reaction system for trapping $\bullet\text{O}_2^-$ and $\bullet\text{OH}$, respectively. (d–e) Ex-situ XPS spectra of C 1s and Ti 2p of Pd/H-TiO₂ under vacuum, CH₄, and O₂ atmosphere and light irradiation. (f) In-situ DRIFT spectra of Pd/H-TiO₂. (g) The proposed catalytic mechanism for the oxidation of methane to methanol over Pd/H-TiO₂.

these, $\bullet\text{OH}$ played an important role in activating methane into $\bullet\text{CH}_3$, and $\bullet\text{O}_2^-$ showed a better performance in further converting $\bullet\text{CH}_3$ into methanol. In sum, new insights into the synthesis of photocatalysts and the mechanism of photooxidation of methane to methanol were provided, which might be useful for future synthesis of high-performance photocatalysts for photooxidation of methane to methanol.

CRediT authorship contribution statement

Xibo Zhang: Conceptualization, Methodology, Software, Data curation, Investigation, Writing – original draft, Writing – review & editing. **Yaqin Wang:** Investigation, Data curation, Validation. **Kuan Chang:** Investigation. **Shuangli Yang:** Investigation. **Huijie Liu:** Methodology. **Qian Chen:** Data curation. **Zhaoxiong Xie:** Resources. **Qin Kuang:** Writing – original draft, Writing – review & editing, Supervision, Funding acquisition, Project administration.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data Availability

Data will be made available on request.

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Declaration of Competing Interest

The authors report no declarations of interest.

Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2022.121961.

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